

534 Rec'd PCT/PTC 26 JUL 2000

HIGH EFFICIENCY RECOVERY PROCESS AND APPARATUS FOR THE PYROLYSIS TREATMENT AND HALO-
GENATION OF MULTI-ELEMENT WASTEFIELD OF THE INVENTION

The field of the present invention is processes for treating and recovering a large variety of types of wastes via chemical treatment.

BACKGROUND OF THE INVENTION

The present recovery and recycling industry must use a defined feed stock as raw material in order to be processed. As a result, the recovery industry must spend huge resources in sorting its wastes storing and warehousing. This is the main reason for the small quantity of waste which is actually being recycled, and the huge amount which is being dumped with catastrophic environmental effects.

Examples of the above are known and obvious, such as special scrap collectors, scrap yard dealers, for each segment of the industry - copper, aluminum, iron, steel, stainless steel, noble metal etc. in the recycling industry on the one hand, and the unlimited amount of waste being dumped by the society every day, on the other hand

However, the recycling industry is dedicated mainly to the industrial waste, which is well sorted and defined to each element. In the event that

00501062 22010650

-2-

the scrap is made of different elements or metals, cheap labor is needed in order to dismantle the different components to the different metals. Examples are found in ship scrap, aircraft, cars and municipal waste. The main problem is, that this process requires cheap manpower that have to work in difficult and hazardous conditions. It has been proven in the developed countries, that manual or automated sorting and dismantling systems are usually not economically feasible and are therefore not a valid solution for treatment of most of the mixed waste.

Indeed many industries do address this issue by constructing equipment which makes recycling easy by use of the dismantling methods, such as used in the automobile industry etc. However, due to the use of many complex materials and the sophistication of parts it becomes almost impossible to re-use these parts or repair them.

The only system that treats unsorted waste, to any degree is the Municipal Incineration system, and even then, the waste must not be contaminated by industrial or Hazardous waste. In this system the waste is being introduced into furnaces and incinerated at elevated temperatures, where hot gases usually produce steam and or electricity. This system actually recovers only the energy of the organic matter via oxidation - incineration. All the inorganic waste remains as ash or sludge and is usually placed in a controlled landfill.

006101 "20101050

There are some other systems that have been developed to recover identified elements from identified feed stock - waste, via different systems, such as molten metals, extraction or chlorination methods. For example, Adelman et al (Proc. Iowa Acad. Sci. (1980) 87 (4), pp129-133) discloses the production of aluminum chloride and silicon chloride from fly ash. In this system recovery of Al, Si, Fe, and Ti via chlorination reaction in a gas fluidized bed reactor is used, to convert the metal in the fly ash to volatile metal chlorides. The best yields are achieved when CO and fluid coke are used as reduction agents. Typically 0.5 - 2 hours of chlorination at temperatures of 750 - 900 degrees to produce volatile metal chlorides.

Burnet et al (Univ. Ky., Inst. Min. Miner. Res., [Tech Rep.] IMMR (1997), IMMR 32-M4-77, Proc. - Ky. Coal Refuse Disposal Util. Semin., 3rd 83-8) discloses a high temperature chlorination method of recovering Al_2O_3 from the non-magnetic fraction of fly ash, in which the non-magnetic fraction of fly ash is mixed with C and chlorinated in a fixed bed. The residual Fe in the ash can be removed as volatile Fe chloride at 400-600°C, with very little Al and Si reaction. The temperature is then raised to 850-950°C where a mixture consisting mostly of volatile Al and Si chloride forms. When the vapors are cooled, solid $AlCl_3$ condenses at 120-50°C. The $SiCl_4$ remains in a vapor state due to its low condensation temp. The $SiCl_4$ can

00610E2-101900

Most wastes contain more than one element and several unknown
contaminates. Most wastes contain both organic and non-organic elements.

000678-100

Chlorination of organic material can produce hazardous, toxic and cancerous elements.

It is a purpose of the present invention to provide a process for destruction of hazardous and/or toxic industrial waste in which the toxic and/or the hazardous compound waste is reduced into less toxic, or non toxic material, and/or less hazardous or non hazardous material, and the size and quantity of said waste is also reduced.

It is a further purpose of the present invention to provide a self-catalytic process in which the matter that exists in the compounded waste is converted and used as a catalyst in a subsequent reaction.

It is a further purpose of the present invention to provide an energy recycling process in which the energy produced by one chemical reaction is consumed in a subsequent chemical reaction.

It is a further purpose of the present invention to provide a wide range recycling process in which almost any waste can be treated: organic, non-organic, metallic or non-metallic, sorted or even unsorted.

It is a further purpose of the present invention to provide a recycling process suitable for recovering the basic elements of the waste introduced thereto, thus obtaining valuable and useful materials.

SUMMARY OF THE INVENTION

The present invention relates to a high efficient recovery process for the treatment of multi-element wastes which comprises the steps of

- a) heat treatment of the waste in the presence of a controlled amount of oxygen;
- b) halogenation of the product of step "a"; and
- c) separation of the metal halide products of step "b".

The term "carbonization" used herein is defined as an operation in which organic material is subjected to high temperature in the presence of a limited amount of oxygen, resulting in the decomposition of said material, and affording, *inter alia*, carbon, CO and CO₂.

The heat treatment described in the above step "a" may be referred to hereinafter as "primary heat treatment".

Optionally, when necessary, the raw waste is mechanically prepared in a process which includes any of the steps of shredding, crushing, milling and briquetting, prior the step of primary heat treatment.

Preferably the primary heat treatment is performed at a temperature of less than about 1000°C.

Preferably, during the primary heat treatment, the waste is agitated.

Preferably, the primary heat treatment is carried out in such a way that any one or more of the actions selected from the group which consists of evaporation of water and/or organic material, carbonization, destruction and/or cracking of organic material, and reduction of metal oxides to metals and/or metal carbides, are achieved.

00610122 101900

According to another embodiment of the present invention, the primary heat treatment is carried out under atmospheric pressure or higher pressures, optionally in the presence of gases, preferably hydrogen, capable of cracking the organic or inorganic material.

Preferably, the halogenation reaction is conducted with mechanical movement between the gaseous halogen and the waste, as fixed fluidized bed vibrating or in walking grid or in rotary kiln.

Preferably, the halogenation reaction is a chlorination reaction, a bromination reaction or a combined chlorination-bromination reaction, and more preferably a chlorination reaction.

Preferably, the halogenation reaction is performed at a temperature in the range between ambient temperature and 1500°C, more preferably between 700°C and 750°C.

Optionally, the halogenation temperature may vary according to the boiling or sublimation point of the metal halide products, as will be hereinafter explained.

Preferably, the separation of the halide products (step "c" above) is by means of any one or more, or any combination of operations selected from

00601032-101500

the group consisting of gaseous or liquid fractional deposition, distillation, filtration, selective chemical vapor deposition (hereinafter CVD), settling, selective oxidation, selective halogenation, selective dissolution and selective extraction, and more preferably by means of gaseous fractional deposition.

Optionally, when desired, the separation stage may be followed by a purification procedure for each of the separated products, to remove impurities therefrom.

Optionally, a portion of the heat energy possessed by the product material of the primary heat treatment may be used in the halogenation, e.g., said product of the primary heat treatment may be transferred from the primary heat treatment chamber to the halogenation chamber when hot, and the halogenation reaction may be started shortly afterwards, and thus it is required to heat the material of the halogenation reaction merely from the temperature which it is at, and is substantially higher than, e.g., room temperature.

Optionally, the activation of metals in the halogenation reaction may be catalyzed by the introduction of the carbon produced during the primary heat treatment and/or of untreated flue-gas including e.g. bromine,

005010E2-101900

Preferably, said fractional deposition system comprises one or more deposition columns wherein each column comprises means of maintaining the temperature thereof at a pre-determined level; said fractional deposition system further comprising an outlet pipe.

According to another preferred embodiment of the present invention, the separation system is a CVD system comprising one or more heated or chilled elements allowing the deposition of the specific metal halide vapors thereon.

Preferably, said outlet pipe comprised in the fractional deposition system is connected directly to the halogenation chamber.

Optionally, said apparatus further comprises one or more units which can perform one or more actions selected from any of the group which consists of shredding, crushing, milling, sludge briquetting, feeding and dosing or any combination thereof, said unit being connected to the inlet of said primary heat treatment chamber and/or to the inlet of said halogenation chamber by means of a conduit.

Preferably, said apparatus further comprises an additional heat chamber, referred to hereinafter as secondary heat chamber, a heat exchanger, a scrubber a filter, a blower and a stack; said additional heat chamber

006101052-101900

-11-

comprising a means of heating, a gas inlet and an air inlet, and a flue gas outlet; said gas inlet of said secondary heat chamber being connected by means of a conduit to the flue gas outlet of said primary heat chamber; said heat exchanger comprising an inlet and an outlet; the flue gas outlet of said secondary heat chamber being connected by means of a conduit to the inlet of said heat exchanger; said scrubber comprising an inlet and an outlet; the outlet of said heat exchanger being connected, by means of a conduit to the inlet of said scrubber;

Preferably, said apparatus further comprises a filter, a blower and a stack; said filter comprising an inlet and an outlet; the outlet of said scrubber being connected, by means of a conduit to the inlet of said filter; said blower comprising an inlet and an outlet; the outlet of said filter being connected, by means of a conduit to the inlet of said blower; said stack comprising an inlet and an outlet; the outlet of said blower being connected, by means of a conduit to the inlet of said stack.

Preferably, said scrubber and said filter are connected to the halogenation chamber by means of conduits, to recycle material recovered and collected by said scrubber and filter to said halogenation chamber.

006101062-101900

DESCRIPTION OF THE INVENTION

The present invention relates to a high efficient process for the treatment of wastes which is applicable in treating mixtures of waste. Said mixtures consisting of a very wide range of chemical elements and compounds, organic and non-organic, in different physical forms, such as solid, liquid and gas. Said process comprises the following steps:

a) Primary heat treatment of the waste:

Said stage optionally includes evaporation of water, evaporation and carbonization of organic matters from the waste in a controlled oxygen atmosphere preferably at a temperature of less than 1000°C, or in metallic molten bath, said bath preferably being at a temperature of between 500°C and 1600°C. In the presence of hazardous waste, a secondary combustion chamber will destroy all remaining organic matters in the flue gas at a temperature of more than 1200°C at minimum of 2 seconds retention time.

The primary heat treatment is conducted at a controlled oxygen level, thus, it may produce controlled and reduced metallic oxides and exchange or reduce the oxygen layer with carbon, and produce carbon residue which acts both as a catalyst in the halogenation reaction and impregnates into a portion the metal phase at elevated temperature which all will facilitate the halogenation reaction.

00501062-101900

In order to improve the productivity of the process according to the present invention and to render it ecologically friendly, the flue gas evolving from said primary heat treatment, which typically contains certain amounts of low temperature vaporized material, is subjected to an air purification procedure, according to techniques known in the art, which are preferably selected from scrubbing and filtration, to recover the desired materials from the flue ash, which materials are recycled and processed in the subsequent halogenation stage.

b) Halogenation of the product of the heat treatment:

Material present in the remainder of the waste and optionally, from other sources as well, and in particular, recycled material obtained upon recovering the flue gas by scrubbing and filtration, as described above, which may include metals, metal carbides, metal oxides, other inorganic material and possibly traces of organic material is halogenated at a temperature between ambient temperature and 1500°C, preferably between 300°C and 1500°C, and more preferably between 700°C and 750°C. The carbon remaining in the waste, together with additional carbon, if required, acts as a catalyst in the halogenation. Preferably, the halogenation reaction is a chlorination reaction, a bromination reaction or a combined chlorination-bromination reaction, and more preferably the halogenation reaction is a chlorination reaction. Preferably, all of the above halogenation reactions are performed in the gaseous phase.

The halogenation reaction may be conducted with various mechanical apparatus such as fluidized bed, vibrating grid, walking grid, rotary kiln and multi chamber.

The primary heat treatment chamber and/or the halogenation chamber of the present invention may be each independently be placed horizontally, vertically or in an angle.

According to one preferred embodiment of the present invention, hereinafter referred to as "selective halogenation", the halogenation reaction is carried out at a first temperature at which only some of the waste materials undergo reaction with the halogen, and upon separating the halides obtained, the temperature is varied and the halogenation of the remaining waste materials is completed, or partially completed, at a second temperature. If desired, the temperature is further varied and the procedure is repeated as many times as required. According to another preferred embodiment, the halogenation reaction is conducted at a temperature at which the halides are obtained in different states of matter, e.g., at a temperature in which one or more halides is a gas, and one or more of the other halides is a liquid or solid. One skilled in the art will appreciate that in the two embodiments described above, the halogenation temperature is an important parameter playing a role in accomplishing the separation of the halide products.

00601062-101900

c) Separation of the halide products: such a separation can be preferably done by means of any one or more, or any combination of separations selected from the group consisting of gaseous or liquid fractional deposition, distillation, filtration, settling, selective oxidation, selective halogenation, selective evaporation, selective dissolution, selective extraction, selective chemical vapor deposition, selective electrical behavior and more preferably by means of gaseous fractional deposition (see, e.g. Zelickman A.N. Nikitina L.L. Moscow 1978).

Gaseous fractional deposition may be performed passing all the volatile chlorides, M_xCl_y , through one or more solidifying columns. Each has a temperature controlled system that maintains accurate conditions of e.g. temperature. The halide with the highest solidifying temperature solidifies in the first column, whereas the remainder of the halides in the gaseous phase pass to the next columns for further solidifying. In each solidifying column, there will be one or more definite halide materials. The resolution of the separation depends on the accuracy of the solidifying temperature and pressure control, and the dynamics of the gaseous flow. The solidified halides of each column may consist of the solidifying of several halides which are further separated, preferably by recycling each group of halides solidified in a certain column to the gaseous fractional deposition system, wherein accurate conditions are used to improve the resolution of the

-16-

separation of the halides which have relatively close solidification temperatures. The substantially definite halides obtained thereby are subsequently preferably purified, to remove impurities therefrom. The final separation and purification steps may be accomplished using known technologies of hydrometallurgy and others, such as forming a solution in water or other liquids and filtration, solidification, CVD, etc. (see, e.g. Zelickman A.N. Nikitina L.L. Moscow 1978)

According to a preferred embodiment of the invention, the separation of the halide products comprises selective halogenation, selective evaporation and selective condensation, in any suitable sequence order and as many sequences as required. According to one preferred embodiment, the halogenation is carried out at a first temperature at which only some of the waste materials are converted to halides (selective halogenation), which halides, at said first temperature, are preferably in different states of matter, e.g., some halides are in the vapor phase while others are in a condensed phase (selective evaporation). The evaporated halides are removed from the reaction mixture, and are subsequently separated, preferably using the differences in their condensation temperatures, e.g., by gaseous fractional deposition (selective condensation) and optionally, additional methods known in the art. The reaction mixture, comprising non-evaporated halides together with waste materials which were not halogenated at said first temperature, such as glass and ceramics, is

006101032-101900

subjected to another separation procedure, to separate the non-evaporated halides therefrom, using methods known in the art, for example, methods based on the differences between the water solubility of said non-evaporated halides and the non-halogenated waste materials. Finally, the non-halogenated waste materials are reacted with halogen at a second temperature, preferably between 900-1500 degrees, or are separated by known hydrometallurgy technologies (see, e.g. Zelickman A.N. Nikitina L.L. Moscow 1978).

Optionally, the raw waste and/or the product of the primary heat treatment is mechanically prepared in a process which includes any one or more of the following steps:

- i) mechanical shaping of solid waste into pieces of a size to suit further equipment and productivity.
- ii) crushing and/or milling of waste;
- iii) briquetting of sludge

According to one embodiment of the present invention, a mixture of 1%-7% bromine in chlorine is used in the halogenation stage in the event that noble metal atoms or compounds such as Ag, Pt and Pd are present.

It is preferable to execute the primary heat treatment at a low as possible temperature in order to substantially reduce the evaporation of metals at said stage and thus reduce particle emission and to obtain an improved recycling efficiency.

005101-22010060

During the process of the present invention it is desirable to control parameters such as temperature of primary heat treatment and of halogenation, mass flow to, from and in the primary heat treatment chamber and halogenator in order to achieve higher efficiency. Thus, the waste movement into and in the primary heat treatment chamber may be adjusted in order to improve evaporation of water and/or organic material, carbonization, destruction and/or cracking of organic material and reduction of metal oxides mechanical reduction of the waste. The temperatures in the primary heat treatment chamber may be adjusted in order to obtain more efficient reaction with carbon, and its diffusion; the waste movement in the halogenator may be adjusted in order to achieve more efficient halogenation; the air flow in the primary heat treatment chamber may be adjusted in order to achieve an optimal carbonization, organic destruction, cracking, metal oxide reduction and halogenation. The chlorination chamber temperature may be adjusted in order to evaporate material having low boiling point or sublimation point and later material having higher boiling point or sublimation point, thus performing separation thereof.

Furthermore, the air flow in to the primary heat treatment chamber may be regulated in order to produce carbon in quantities required for optimal halogenation.

00601052-101900

00601062 "101900

An advantage of carbonization resulting in incomplete combustion over that resulting in complete combustion is that the former results in less gasses than the latter, most of the organic matter is cracked into carbon and hydrogen molecules, the formation of CO and CO₂ molecules is substantially reduced. The gas flow in incomplete combustion is reduced in temperature, volume and velocity, which substantially reduces the particle emission and simplifies the treatment of the flue gas which consists of heat exchanging, heat recovery and emission control. The lower temperature reduces the amount of volatile inorganic matter in the flue gas. The lower velocity of the gas flow reduces the amount of particles drawn. The substantial reduction of in-flow of air usually required for said incomplete combustion can reduce the amount of emitted flue gas. The volatile organic matter only, can be further incinerated in the secondary chamber, however, said gas will require less oxygen for its incineration and will be almost free of non-gaseous particles. All the above renders the system more environmental friendly especially regarding the "greenhouse effect".

In the event that any of the various fractions of the metal halides which were deposited in the fractional deposition contains a mixture of halides, said mixture may be further separated and purified by known hydrometallurgy technologies and by further fractional deposition of higher resolution.

Most of the waste is recycled by decomposing the material to its basic elements or their halide / oxide derivatives.

The process of the present invention being self-catalyzed, requires little or no addition of material for the purpose of catalysis. According to the present invention, use as catalysts in the recycling phase, is made of elements which exist in most of the wastes to be treated, thus the introduction of catalysts *per se* to the process is minimized.

BRIEF DESCRIPTION OF THE DRAWING

Fig. 1 schematically illustrates an apparatus for a high efficient process for the treatment of multi-element wastes according to the present invention.

DETAILED DESCRIPTION OF PREFERRED EMBODIMENTS

According to one embodiment of the present invention, the scrap to be treated is inserted to a shredder, 1, and shredded therein. The shredded scrap is loaded by means of a ram loader, 2, into the rotary heat treatment chamber, 3, and the primary heat treatment is performed therein. The gaseous material exiting the primary heat treatment chamber flows to the secondary combustion chamber, 5, where all matters are combusted at an elevated temperature. Additional air is introduced through regulated vent (17). The hot flue gas flows to the heat exchanger (8) into which water is introduced through conduit (7) and withdrawn as a hot stream through

00601062-101900

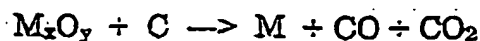
-21-

conduit (18). The chilled flue gas passes through scrubber (6), where any gaseous emission is absorbed by caustic or lime. The flue gas further passes through the filter bag (4), to remove any particles. The filtered flue gas is released to the atmosphere by means of blower (19), through stack (20). The formation of high pressure within the system is prevented by means of valve (17) and blower (19). The non-gaseous material remaining from the primary heat treatment and the material recovered by the air purification procedure, i.e., the particles collected in the filter bags and the scrubber residues, are introduced into the halogenation chamber, 9, through valve, 21, which is closed during the halogenation reaction. Halogen compounds such as chlorine, bromine or a mixture thereof are introduced to the halogenation chamber via conduit 10. Condensation columns 11, 12, 13, 14 and 15 are maintained accurately at temperatures T_1 , T_2 , T_3 , T_4 and T_5 , accordingly, under the condition that $T_1 > T_2 > T_3 > T_4 > T_5$, and at an accurately controlled pressure. The gaseous product of the halogenation reaction is passed through said condensation columns, and the metal halides deposit thereon according to their characterized deposition temperature, and are collected and thus separated. The remaining gas which comprises excess halogen gas exits the apparatus through conduit 16. The non-gaseous material which remained in the halogenation chamber is collected and separated if required. Said remaining gas of the halogenation reaction may be recycled back into the halogenation chamber.

00501062-101900

According to a preferred embodiment of the present invention metal scrap/waste is reduced to a size that can be introduced to the equipment. Organic waste is treated in a controlled atmosphere or in a molten metallic phase with an oxygen deficiency in order to maintain carbon particles which will serve as catalysts and also reduce the oxide layer on the metallic waste. The gas streams pass through an air-controlled abatement system. The heated inorganic waste or the molten mixture with carbon, if necessary, are then fed to a halogenation reactor either - vertical, horizontal, fixed or fluidized bed. Additional carbon is introduced if needed. The carbon residue from the incineration process is used as a catalyst for the halogenation process.

According to a preferred embodiment, most of the metallic scrap is oxidized after a certain time of being exposed to the air, humidity and sun. This causes a problem to the extent that the oxide layer acts as a passive layer which deactivates the chlorination process. Said problem can be solved according to the present invention by the controlled incineration with oxygen deficiency at elevated temperatures of between 300°C and 1050°C, preferably between 800°C and 850°C. Thus, in the presence of a sufficient amount of carbon in the incinerator, the metal oxides and carbon may be converted to metals and CO and CO₂ according to the following empirical formula:



09601062-101900

000001052 101 0000

According to a preferred embodiment of the present invention, the gas flow resulting subsequent to the fractional deposition process, which contains a high percentage of halogen gas, may be recycled back into the halogenator.

Example 1

500 Grams of unsorted automobile scrap was introduced to the process of the present invention as follows: At first said scrap was shredded to pieces of a length of approximately 10mm. Said pieces were carbonized (in the

-24-

absence of oxygen) at a temperature of between 600°C-700°C for about 1 hour. Table 1 shows the content of said scrap before and after carbonization.

NAME	ELEMENT CONTENT (wt%)											
	Fe	Al	Cu	Ni	Mg	Co	Sn	O	Organic	noble metal	Wgt	%
Scrap before carbonization	53	18	4	2	4	15	13	5	11	0.05	500	100
Scrap after carbonization	61	21	4.5	2.0	4.6	17	15	-	2.4 carbon	0.05	432	86.4

Table 1

The carbonized material was further chlorinated at a temperature of about 750°C, and the various metal chlorides were separated. Table 2 shows the content of the material after the chlorination reaction.

ELEMENT CONTENT (%)										
Weight (gr.)	FeCl ₃	AlCl ₃	SnCl ₄	NiCl ₂	CuCl	CoCl ₂	noble metal	MgCl ₂	Conden. Chamber	Conden. Temp(°C)
	771			0.18					II	250-300
		440							III	1000
			14.2						IV	50
				14.5					I	600
130	4.26			8.5	28.5	15	0.46	78.3	V	
total: 1370	775.26	440	14.2	18.18	28.5	15	0.46	78.3		

Table 2

Example 2

600 Grams of crushing electronic scrap was introduced to the process of the present invention as follows: At first said scrap was shredded to pieces of a

-25-

length of approximately 10mm. Said pieces were carbonized (in the absence of oxygen) at a temperature of between 650°C-700°C for about one hour.

Table 3 shows the content of said scrap before and after carbonization.

NAME	Cont. Element %													
	Fe	Cu	Ni	Sn	Pb	Zn	Co	As	Ag	Pd	O	Org.	C	Wt
Scrap before Carbonization	6	20	2.5	3.0	2.0	3.0	0.25	0.025	0.15	0.018	6	56	-	600
Scrap after Carbonization	13	44	5	11	4.4	6.6	0.5	0.055	0.83	0.04	-	2.5	4.0	270

Table 3

The material treated by means of primary heat treatment was chlorinated at a temperature of about 250°C for about 3 hours, and the various metal chlorides were separated. Table 4 shows the content of the material after the chlorination reaction.

NAME	Wgt.	FeCl ₃	SnCl ₄	NiCl ₂	ZnCl ₂	CoCl ₂	CuCl	PtCl ₂	AsCl ₃ g/t	Ag g/t	Pd
Chloride iron FeCl ₃		101									
Chloride Tin SnCl ₄			61.0								
Chloride Nickel NiCl ₂				23							
Chloride Zinc ZnCl ₂					32						
Residue in Chlorinator	198			5.0	3.5	2.7	173	14.2	0.061 %	0.17%	0.058%
Total	415	101	61.0	28	35.5	2.7	173	14.2			

Table 4

Example 3

200 Grams of mixture of spent catalyst waste were introduced to the process of the present invention as follows: Said waste was treated by means of primary heat treatment, in the absence of oxygen, at a temperature of about 650°C for about 1.5 hours. Table 5 shows the content of said waste before and after primary heat treatment.

NAME	Cont. element %								
	Weight total	WO ₂	Ta ₂ O ₅	TiO ₂	Co ₂ O ₃	Organic	C	SiO ₂	Al ₂ O ₃
Scrap before Calcination	200 gr	38	9	31.0	3.5	20	-	24	14
Scrap after Primary heat treatment	100	W 31	Ta 7	31.0	Co 2.2	-	4.5	16	8

Table 5

100 Grams of the calcinated material were chlorinated at a temperature of about 700°C, for about 2 hours, and those from among the various metal chlorides which were evaporated at said temperature, were removed from the reaction mixture and subsequently separated in condensation columns, due to the differences in their condensation temperature. Table 6 shows the content of the material after the chlorination reaction. Alternatively, the evaporated metal chlorides may be all condensed at 20°C on one column, and may be subsequently separated upon raising the column temperature, due to their differences in their evaporation temperature.

NAME	Weight	WCl ₅	TaCl ₅	TiCl ₄	CoCl ₂	SiO ₂	Al ₂ O ₃	Halogen. T °C)	Evapo. T °C)	condens. T °C)
WCl ₅		64						650	350	200-250
TaCl ₅			9.0					650	240	200-250
TiCl ₄				122				450	136	0-20
CoCl ₂					4.6			500	900	500
SiO ₂						14		900	950	500
Al ₂ O ₃							6.8	900	950	500
Residue in Chlorinator	25.0				4.6	14	6.8			
Total	245	64	9.0	122	4.6	14	6.8			

Table 6

006T0T 290T0950

-27-

The remaining residue in the chlorinator comprised a non-evaporated halide (CoCl_2) and two oxides, which did not undergo chlorination at 700°C . The CoCl_2 was separated from SiO_2 and Al_2O_3 , e.g. according to the principle of differences of solubility in water as described in the following equation:



The remaining SiO_2 and Al_2O_3 were introduced to a chlorination chamber at 950°C and were converted to AlCl_3 (18g) and SiCl_4 (32g).

Example 4

The primary heat treatment of Example 3 was repeated, and 100g of the material treated by means of primary heat treatment was chlorinated at a temperature of about 900°C , for about 1.5 hours, and the various metal chlorides were separated. Table 7 shows the content of the material after the chlorination reaction.

NAME	Weight	CoCl_2	WCl_5	TaCl_5	AlCl_3	TiCl_4	SiCl_4
Chloride Cobalt - CoCl_2		4.7					
Chloride Tungsten - WCl_5			64				
Chloride Tantalum - TaCl_5				9.0			
Chloride Aluminum - AlCl_3					18		
Chloride Titanium - TiCl_4						122	
Chloride Silicon - SiCl_4							32
Residue	6.0				Al_2O_3 2.5		SiO_2 8.5

Table 7

Example 5

006101052-101900

A mixture of 100g of Nickel-Cadmium batteries was introduced to the process of the present invention as follows: At first said scrap was shredded to pieces of a length of approximately 1-5cm. Said pieces were calcinated (in the absence of oxygen) at a temperature of about 650°C, for about 3 hours.

Table 8 shows the content of said scrap before and after primary heat treatment.

Type of scrap	% Ni	%Cd	%Fe	% Organic Silicon
Before Primary heat treatment	20	14	32	34
After Primary heat treatment	24	16	34	SiO ₂ - 16; C - 20

Table 8

The material treated by means of primary heat treatment was chlorinated at a temperature of about 650°C, for about 1.5 hours, and the various metal chlorides were separated. Table 9 shows the content of the material after the chlorination reaction.

NAME	Weight	FeCl ₃	NiCl ₂	CdCl ₂	SiO ₂	C
Chloride Iron FeCl ₃		96				
Chloride Nickel NiCl ₂						
Chloride Cadmium CdCl ₂						
Residue in Chlorinator	101		49	26	16	10

Table 9

While some embodiments of the invention have been illustrated, it will be clear that the invention may be carried out by persons skilled in the art with many modifications, variations and adaptations, without departing from its spirit or exceeding the scope of the claims. Thus, e.g., the invention may be applied to scrap or apparatus different from that herein described.

00501062 "1015000